WAYS TO USE WASTE-FREE TECHNOLOGY IN THE PRODUCTION OF SODA PRODUCTS

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ANNOTATION

The ammonia method of soda production generates a large amount of liquid and smoky gaseous waste. Disinfection of these wastes is an urgent task in the chemical industry. The article recommends using a membrane separator device to extract limestone and separate the burner from exhaust gases to extract carbon dioxide, as well as using sodium hydroxide instead of lime milk to extract ammonia. Such a solution prevents the release of gaseous waste into the environment, and instead of liquid waste, a solution of sodium chloride is obtained, which is reused in production. In addition, the consumption of water, sodium chloride, electricity and fuel is significantly reduced, and the profitability of production increases.

Keywords: soda ash, ammonia method, distilled liquid, exhaust gases, membrane technology, membrane separation.

Today, the most common method of producing soda ash in the chemical industry is the dissolution method or the ammonia method. The ammonia method is based on the following reaction [1]:

$$NaCl + NH_3 + CO_2 + H_2O \leftrightarrows NaHCO_3 + NH_4Cl$$

Since carbon dioxide is poorly soluble in water in the absence of ammonia, sodium chloride salt solution is first ammoniated in the absorption compartment with partial absorption of CO_2 , while ammonia passes into the bound form $(NH_4)_2CO_3$, NH_4HCO_3 , NH_4Cl , NH_4COONH_2 , NH_4OH). Since ammonia is constantly processed in production, its regeneration is carried out by thermal decomposition of salts (at a temperature of 70-100°C). However, ammonium chloride does not decompose at certain temperatures, and in traditional production it is disposed of with lime milk $Ca(OH)_2$. At the same stage, the main waste products are formed– $CaCl_2$ solution or distilled liquid:

$2NH_4Cl + Ca(OH)_2 = 2NH_3 + 2H_2O + CaCl_2$

About 9-10 m³ of distilled liquid (suspension) containing about 100 g/l CaCl₂, 50 g/l NaCl, Ca(OH)₂ and CaCO₃ is formed per one ton of the resulting soda [2]. Solids are released from this stream, and the liquid phase is ejected as a liquid stream. This waste stream mainly contains

calcium and sodium chlorides[3]. Dumping of these wastes into reservoirs leads to their excessive mineralization and solidification, which harms the environment.

Due to the constant tightening of environmental safety requirements and the irrational use of material resources, this problem is becoming more and more urgent in the world. Methods of recycling these wastes are being developed, but due to their large amount, they continue to drain into nearby reservoirs or accumulate in mud reservoirs (sedimentary ponds or «white seas»). The authors of this article have developed a technical and economic analysis of waste-free production of soda ash by the ammonia method.

For production, carbon dioxide is proposed to be obtained partly from soda ash, which is formed in furnaces during production as a fuel combustion product, or partly from exhaust gases that can be obtained from nearby industries (instead of traditional extraction and burning of limestone). This significantly reduces carbon dioxide emissions into the environment. An additional advantage of this technology is the reduction of emissions into the atmosphere. Carbon dioxide can be isolated using membrane separation methods.

The difference between the proposed technology and the traditional scheme of replacing a limestone incinerator with a membrane one: the exhaust gases are condensed, then cooled and transferred to a membrane separator unit, purification from which is about 40%. The CO₂ is directed into the absorption columns against the carbonation section. Membranes with high selectivity of CO_2/N_2 gas separation are presented on the chemical industry market today [4].

Traditional methods of absorption separation of CO_2 are not used due to its low concentration in exhaust gases and large gas flows, since CO_2 removal devices must be large-scale and energyintensive.

The use of membrane separation to remove carbon dioxide from exhaust gases leads to the formation of a by-product - technical nitrogen (97%). It can be used for fire extinguishing systems, cleaning pipes, testing them and refuelling cars.

Since in this technological scheme there is no need to prepare lime milk Ca(OH)₂ for mining, burning limestone and, accordingly, decomposition of ammonium chloride, it is recommended to replace calcium hydroxide with sodium hydroxide NaOH:

 $NH_4Cl + NaOH = NaCl + H_2O + NH_3$

Thanks to this technical solution, instead of a large amount of liquid waste discharged into sedimentary wastewater, the reaction product is a sodium chloride solution that can be regenerated during full production. At the same time, the consumption (consumption) of water and the purchase of sodium chloride are significantly saved. Due to the absence of a limestoneburning workshop, the consumption of electricity and fuel is significantly reduced.

A preliminary technical and economic analysis of the proposed technology showed that the enterprise, built based on the proposed technology, will fully recoup the costs incurred within 4.6 years.

Thus, due to the use of this technology, the amount of both liquid and gaseous waste is reduced at the enterprise, which allows saving about 450 m³ of carbon dioxide and 12 m³ of distilled liquid per year for each ton of soda produced using traditional technology. Since there is no need for limestone mining and sodium chloride consumption, such production can be located far from large natural deposits, next to factories that consume soda ash.

REFERENCES

1. Шатов А.А. Производство кальцинированной соды - от прошлых к новым технологиям // Научное обозрение. Фундаментальные и прикладные исследования. – 2017. – № 1

2. Балевская Я. Д. Технология безотходного производства кальцинированной соды с применением мембранной технологии/ Молодой ученый. -2018. -№ 48 (234). -С. 9-12. –URL: https://moluch.ru/archive/234/54259/

3. Новиков В.Кунградский содовый завод стал производить «тяжелую» кальцинированную cogy.–URL:https://nuz.uz/ekonomika-i-finansy/1158717-kungradskij-sodovyj-zavod-v-

uzbekistane-stal-proizvodit-tyazheluyu-kalczinirovannuyu-

sodu.html?ysclid=lqevy2t239165549133

4. Куканбоев И.И. Технология производства среднетемпературного обессеренного катализатора конверсии оксида углерода (II) водяным паром: Дисс. кан. техн. наук. – Ташкент, 2008. -с.78

5. Таджибоев Д.Р., Куканбоев И.И. Влияние добавки хрома на средне темературного катализатора. Наука молодых будущее России: сборник научных статей Международной научной конференции перспективных разработок молодых ученых (15-16 декабря 2016 года), в 3-х томах, Том 1. Курск: ЗАО Университетская книга, 2016, -С.407 (165-167 с.)

6. Турсунова Г. В., Исаков М. Ю., Содиков М. У., Куконбоев И. И. О результатах исследования азотистых оснований Ферганской нефти. Молодежь и XXI век-2015. 2015. -С. 48-49

7. Batirovna, K. D., Yusupovna, S., & Tolibjonovich, M. I. (2022). Research of the chemical composition of perfumery products. Spectrum Journal of Innovation, Reforms and Development, 9, 271-277.

8. Нуъмонов, Бахтиёржон Омонжонович, etal. "Преципитат и сульфоаммофос на основе конверсии фосфогипса с диаммофосной пульпой." Химическая промышленность сегодня 1 (2021): 34-45.

9. AM Jumanov, HS Tolibjonovna Forming ecological thinking in students on the basis of interdisciplinary relationships //Web of Scientist: International Scientific Research Journal 3 (8), 241-244

10. Ахадов, М. Ш., Каримова, Д. Б., & Орифова, З. З. (2018). Мониторинг HF в атмосферном воздухе. In European research: innovation in science, education and technology (pp. 20-21).

11. Каримова, Диловар Батировна. "Классификация парфюмерной продукции на основе THBЭД." Life Sciences and Agriculture 2-2 (2020): 6-10.

12. Н.Р.Азимова, Б.Е.Абдуганиев, and Д.Б.Каримова "Классификация никотинсодержащей продукции на основе ТНВЭД" Ученый XXI века, №5. 2 (86). 2022. Pp.40-42.